

least an integrated hydrocarbon co-catalyst within the porous framework,
and

- B4
- (b) contacting the silicoaluminophosphate molecular sieve containing the integrated hydrocarbon co-catalyst with an oxygenate feedstock under conditions effective to convert the feedstock to the olefin product, wherein the silicoaluminophosphate molecular sieve has a catalytic activity index for methanol conversion at 250°C of at least 2.
-

27. A method of making a polyolefin from an oxygenate feedstock, comprising:

- B5
- (a) contacting a silicoaluminophosphate molecular sieve having a porous framework structure with a hydrocarbon at conditions effective to form at least an integrated hydrocarbon co-catalyst within the porous framework,
- (b) contacting the silicoaluminophosphate molecular sieve containing the integrated hydrocarbon co-catalyst with an oxygenate feedstock under conditions effective to convert the feedstock to an olefin product, and
- (c) contacting the olefin product with a polyolefin-forming catalyst under conditions effective to form the polyolefin,

wherein the silicoaluminophosphate molecular sieve containing the integrated hydrocarbon co-catalyst has a catalytic activity index for methanol conversion at 250°C of at least 2.

Please add the following new claims:

- B6
51. (New) The method of claim 17, wherein step (a) contacting occurs at a lower temperature and step (b) contacting occurs at a higher temperature.
52. (New) The method of claims 51, wherein a difference between said higher temperature and said lower temperature is at least 10°C.
53. (New) The method of claims 51, wherein a difference between said higher temperature and said lower temperature is at least 25°C.

54. (New) The method of claims 51, wherein the hydrocarbon contacted in said first contacting is different from that contacted in said second contacting.
55. (New) The method of claims 54, wherein a difference between said higher temperature and said lower temperature is at least 10°C.
56. (New) The method of claims 54, wherein a difference between said higher temperature and said lower temperature is at least 25°C.
57. (New) The method of claim 27, wherein step (a) contacting occurs at a lower temperature and step (b) contacting occurs at a higher temperature.
58. (New) The method of claims 57, wherein a difference between said higher temperature and said lower temperature is at least 10°C.
59. (New) The method of claims 57, wherein a difference between said higher temperature and said lower temperature is at least 25°C.
60. (New) The method of claims 57, wherein the hydrocarbon contacted in said first contacting is different from that contacted in said second contacting.
61. (New) The method of claims 60, wherein a difference between said higher temperature and said lower temperature is at least 10°C.
62. (New) The method of claims 60, wherein a difference between said higher temperature and said lower temperature is at least 25°C.
63. (New) The method of claim 17, wherein step (a) contacting occurs in a pretreatment zone and step (b) contacting occurs in a reaction zone.
64. (New) The method of claim 17, wherein step (a) contacting occurs in a pretreatment vessel and step (b) contacting occurs in a reaction vessel.
65. (New) The method of claim 27, wherein step (a) contacting occurs in a pretreatment zone and step (b) contacting occurs in a reaction zone.